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#### **Agenda**

- Life Cycle Costs
- · Design and Engineering Considerations
- · Life Cycle Cost Example
- Factors Affecting Power Usage
- Systems Resistance Curve
  - Velocity
  - Viscosity
  - Flow Regime (laminar, turbulent, or transitional)
- Changing the Systems Resistance Curve
  - Heating
  - Diluent
  - Emulsion
  - Drag Reducers
- Power Optimization Practices
- Additional Discussion



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#### Life Cycle Costs

- Also called "whole life" costs
- Total cost over the useful life of the asset usually expressed in costs per unit (barrel or cubic meter)
- Estimated in the project feasibility stage; updated during Front End Engineering and Design (FEED)
- Remaining life cycle costs can also be estimated starting at any point in the asset's life
- Used for evaluating investments and optimizing costs
- Includes the cost of acquisition, operation, maintenance, conversion, and decommissioning
- Cost streams are normally discounted to time zero to account for the time value of money



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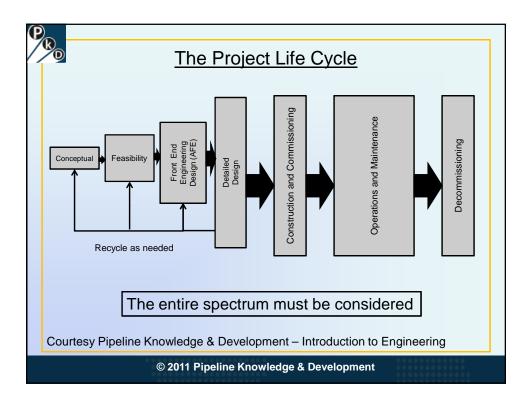
#### <u>Items Comprising Pipeline Life Cycle Costs</u>

- Capital investments
  - Known future investment requirements are considered
  - Past investments are not considered unless they can be sold to bring in money.
- · Operating costs
  - People
  - Power
  - Other
- Maintenance costs
- · Decommissioning and disposal costs

Each of these is important and at least partly influenced by the others.



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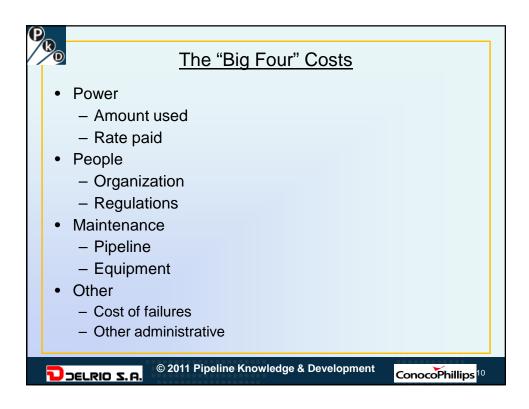
# Design Basis Document Contains the Parameters

- Design capacity (flow rate where design is to optimized)
- Operating range (range of expected flow rates)
- Fluid properties (density, viscosity, specific heat)
- Operating temperature range
- Applicable codes and standards
- Process control philosophy
- Preliminary route receipt and delivery locations
- Sensitivities regarding customers, regulators, public opinion, geological, environmental, or other considerations which would affect line design or routing,
- Project economics and economic sensitivities
- · Special operating considerations

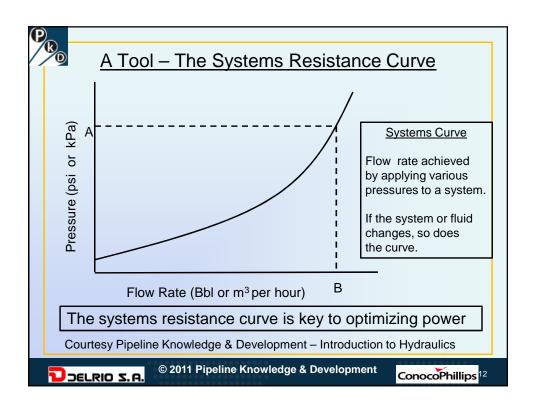


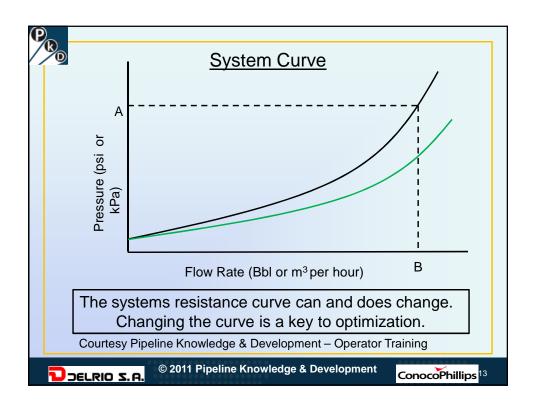
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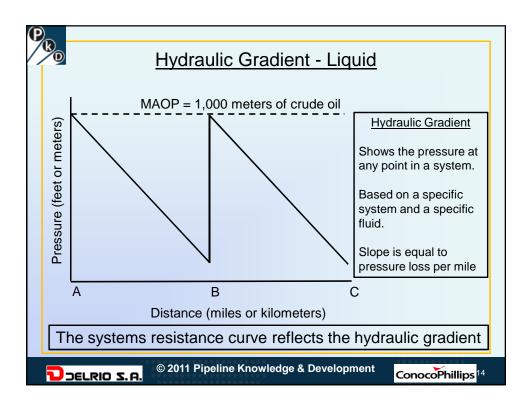
	12-inch	16-inch	20-inch
Total pressure required	6,000 psi	2,000 psi	700 psi
Number of stations required	5	2	1
Pressure per station	1,200 psi	1,000 psi	700 psi
Pipeline investment	\$12,000,000	\$16,000,000	\$22,400,000
Station investment	\$5,550,000	\$2,100,000	\$1,000,000
TOTAL INVESTMENT	\$17,550,000	\$18,100,000	\$23,400,000
Annual operating costs	\$686,000	\$353,000	\$244,000
Depreciation			
- Pipeline @3%	\$360,000	\$480,000	\$672,000
- Stations @4%	\$220,000	\$84,000	\$40,000
- Property taxes @1%	\$175,000	\$181,000	\$234,000
TOTAL ANNUAL COSTS (present value)	\$1,441,000	\$1,098,000	\$1,190,000
Annual cost per unit of capacity	\$0.079	\$0.060	\$0.065

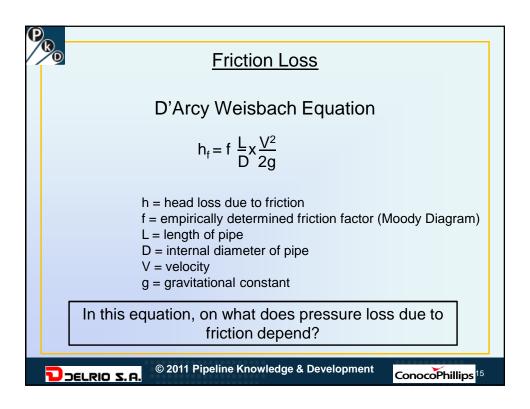


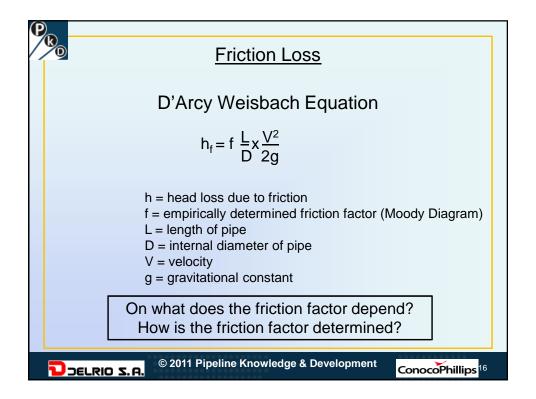
#### Factors Affecting Power Usage Absolute elevation change between points; Fluid characteristics density - viscosity Velocity **Pipeline** - Length - Diameter Internal pipe roughness Configuration of pump and other stations Operating practices Equipment efficiency © 2011 Pipeline Knowledge & Development ConocoPhillips 11 JELRIO S.A.

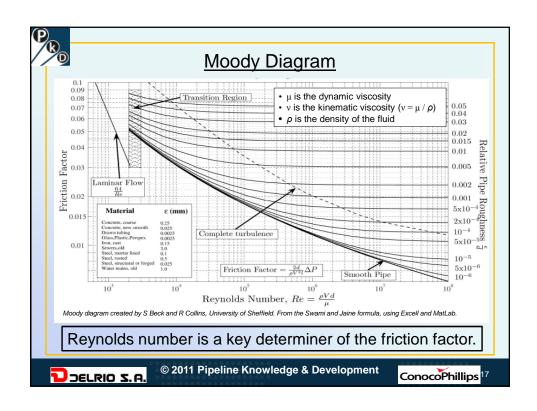


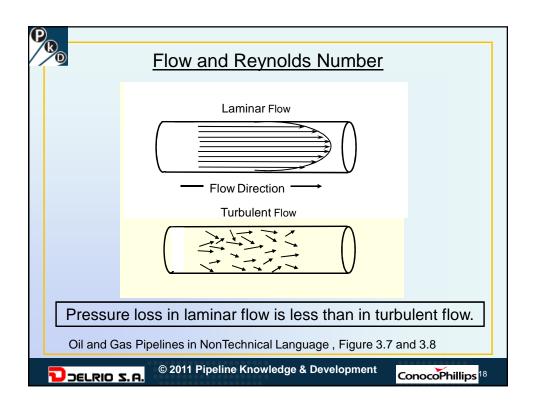


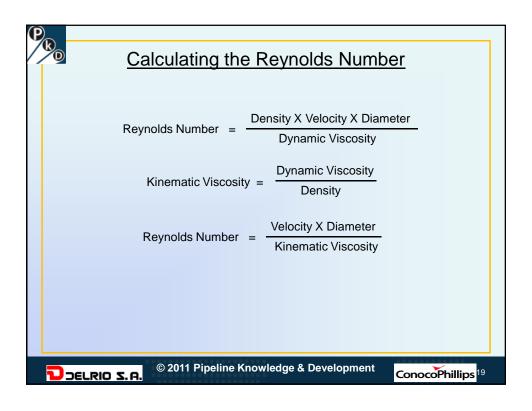


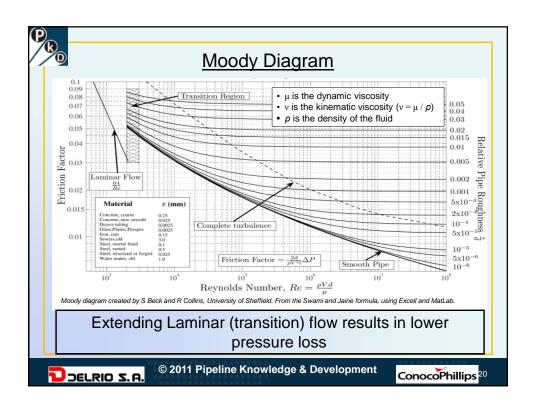


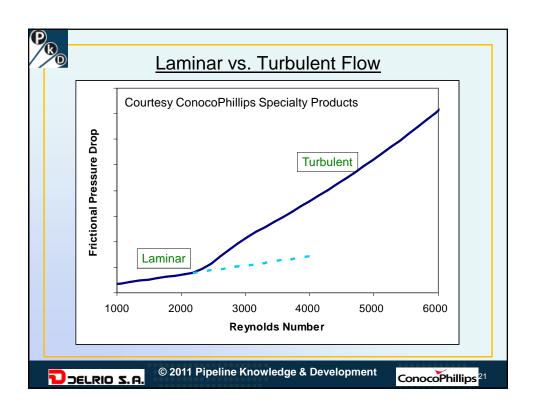


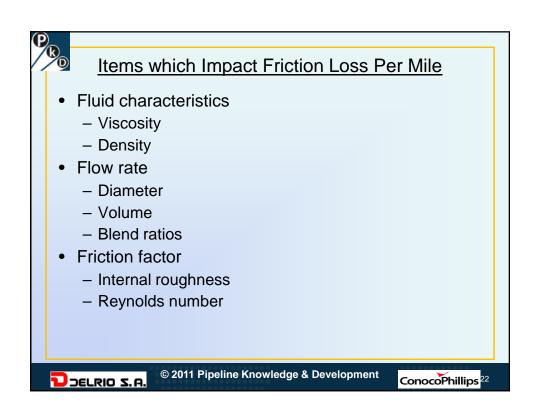


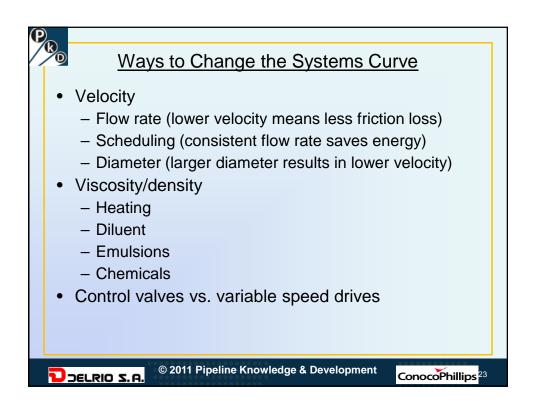


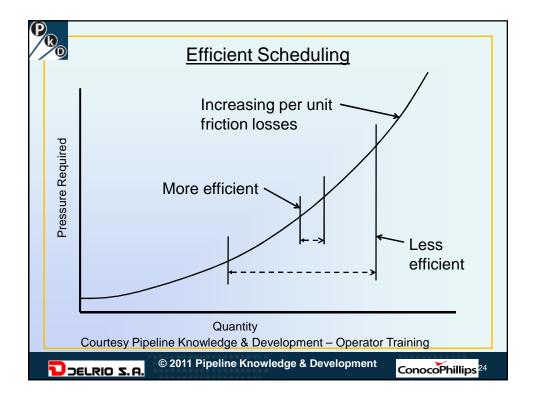


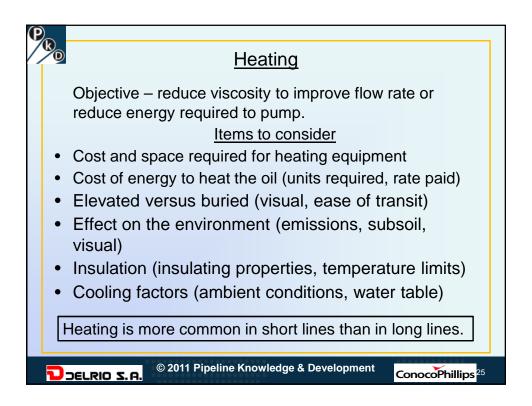


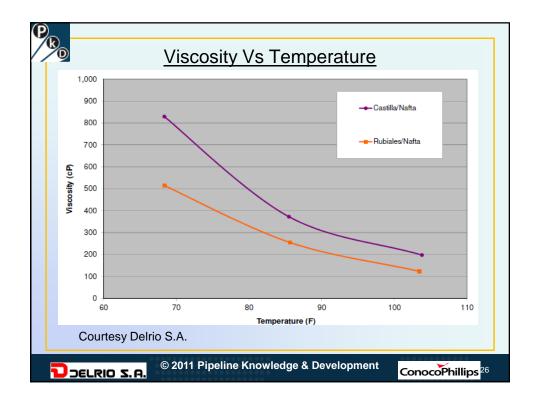


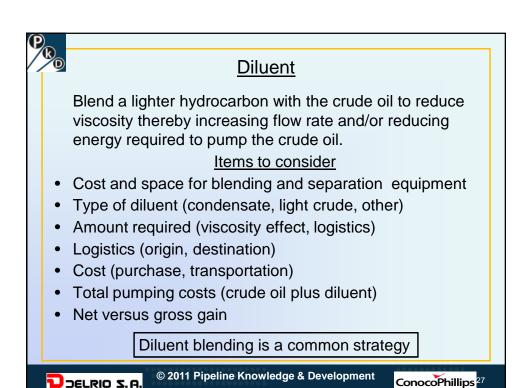


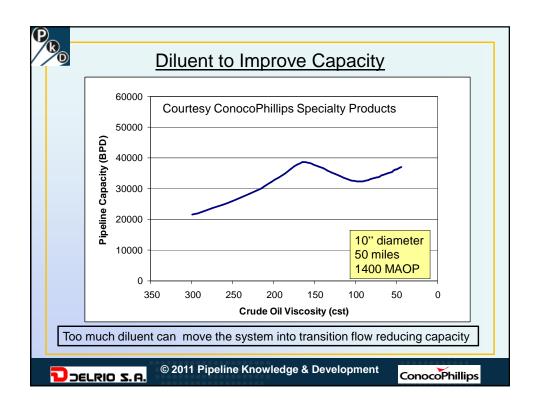














#### **Emulsions**

Create an oil/water emulsion to bring down the overall apparent viscosity thereby reducing the friction loss.

#### Items to consider

- Cost and space for blending and separation equipment
- Optimum blend percentages
- How to ensure water does not drop out
- Amount required (viscosity effect, logistics)
- Logistics (origin, destination)
- Cost (purchase, transportation)
- Total pumping costs (crude oil plus water)



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#### **Chemicals (Drag Reducers)**

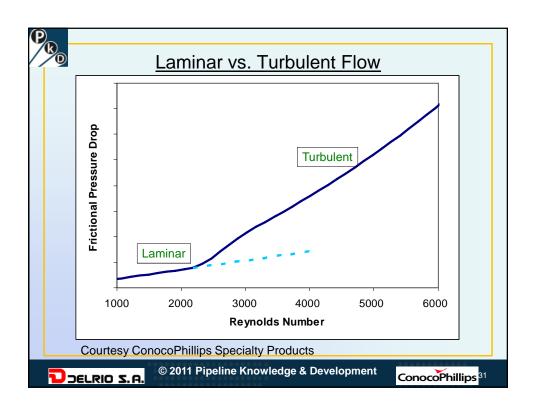
Inject drag reducer into the crude oil to reduce the friction loss per mile thereby increasing flow rate and/or reducing energy required to pump the crude oil.

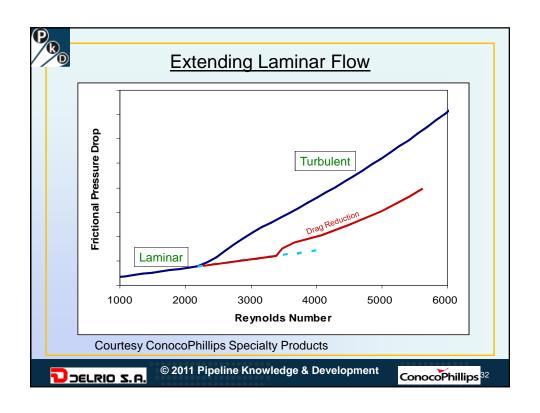
#### Items to consider

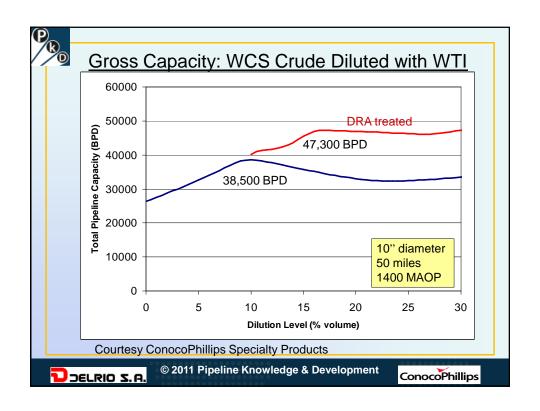
- Drag reduction needed
- Where and how often to inject
- Logistics (equipment, shipping)
- Cost (purchase, transportation)
- Total pumping costs (crude oil plus water)
- Pipe restrictions (pig traps, pipe diameter changes, less than full port values, elbows bends)
- SCADA to control DRA rates (remote vs. local manual)

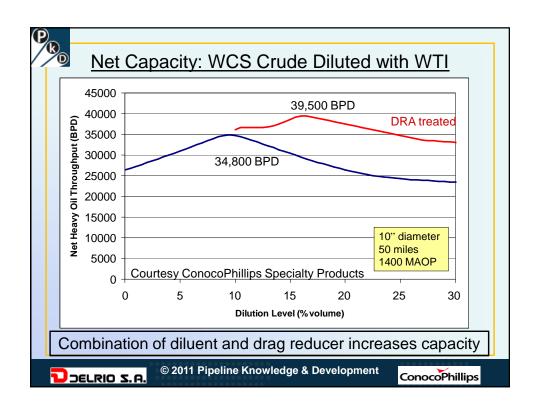


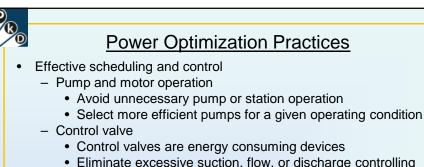
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- Control valves are energy consuming devices
- · Eliminate excessive suction, flow, or discharge controlling
- Flow rate If schedule allows, pump at a lower rate with the minimum number of pumps on-line
- DRA Optimize liquid properties; implement pre-determined schedule when the right mix of crude is being transported.
- Equipment
  - Size pumps, motors, valves, and for system operating conditions
  - Consider VFDs as an alternative to control valves
  - Properly maintain equipment
  - Tune pumps to maximize efficiency

Courtesy Pipeline Knowledge & Development - Operator Training

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